



초공동 유동해석 기술

Numerical Analysis of Supercavitating Flow

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초공동 기술 토의,

2019.04.23

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2. Governing equations & Numerical method

3. Results and discussion

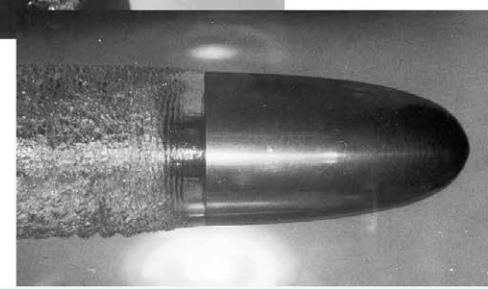
4. Conclusions

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Cavitation

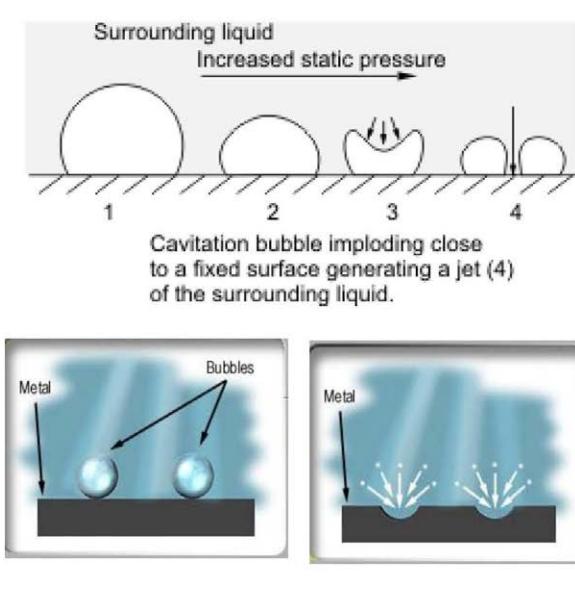
- Widely observed in various propulsion systems and high-speed underwater objects, such as marine propellers, impellers of turbomachinery, hydrofoils, nozzles, injectors and torpedoes.



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Erosion by Cavitation Bubble



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Drag Reduction

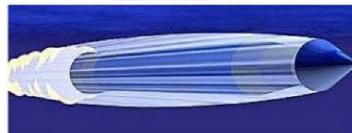
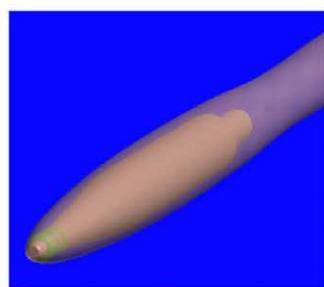


Torpedo Speeds

- Mk-46 Torpedo : 45 knots (80km/h)
 - Shkval I : > 250 knots (450km/h)
 - Shkval II : > 350 knots (rumored 720 knots)
 - Barracuda : > 360 knots (rumored 800 knots)
- 1,440km/h



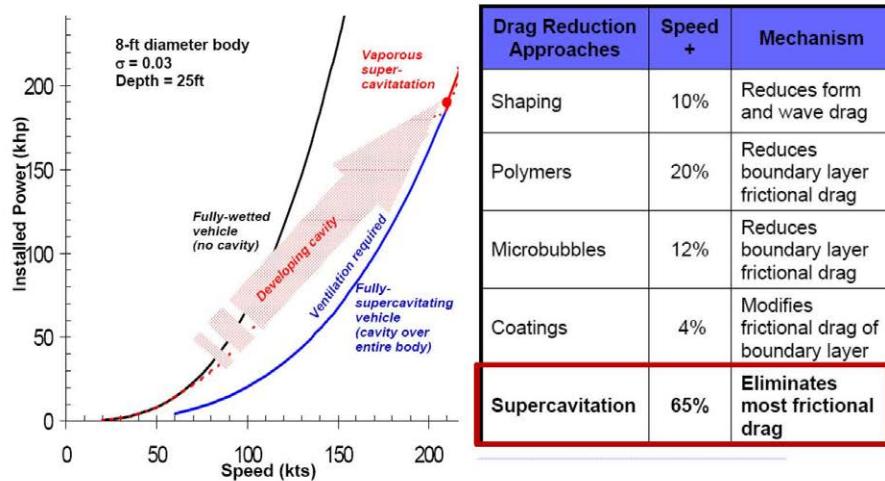
초월공동어뢰



2005 American Controls Conference
Portland, OR June 10, 2005

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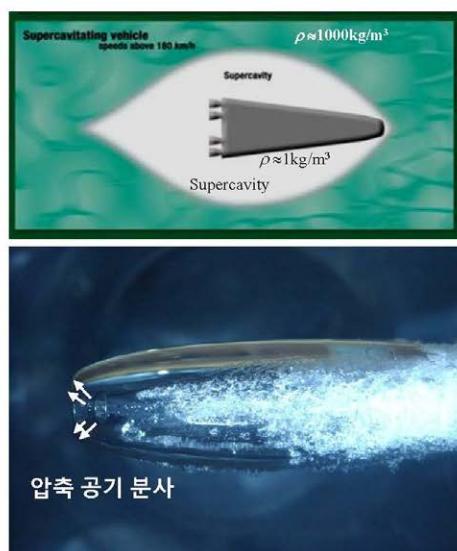
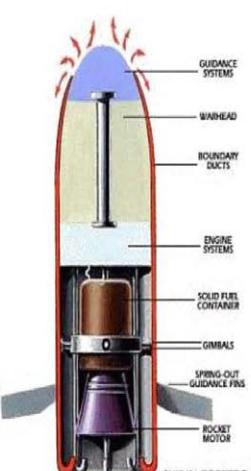
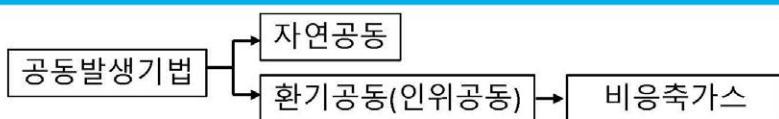
Drag Reduction



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Drag Reduction



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Drag Reduction

Underwater Express / SST (Super-fast Submerged Transport)

Speed ~100 knots

Size : 8 ft dia., 60 tones

- Comparable in size to current special purpose craft such as the MK V Special Operations Craft and the Advanced SEAL Delivery Vehicle

- Mark V: 82 feet long aluminum monohull surface craft, 40 knots

Demonstrate stable and controllable high-speed underwater transport through supercavitation for future littoral missions

Period : Nov. 2007 ~ 2010

Monitored by DARPA / ATO

Northrop Grumman Team selected

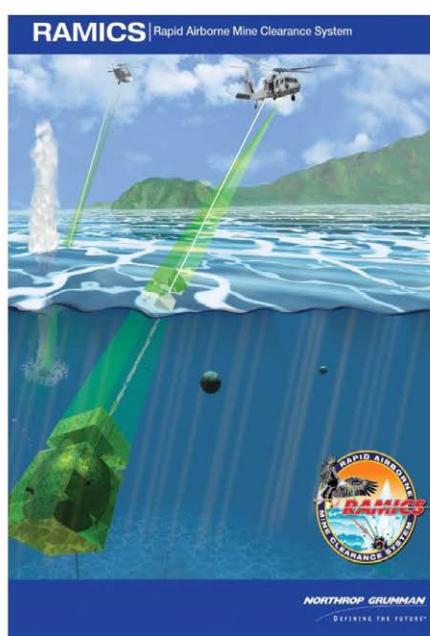
(\$45.8 million for 3 phases, ~4 years)



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Drag Reduction



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Supercavitating bullet

30 mm Underwater Firing Fixture



Typical Launch



Safety Containment



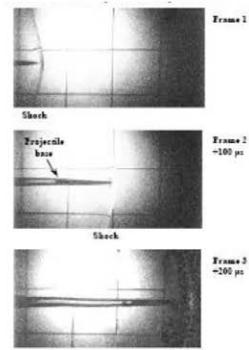
Undersea Gun

NUWC UNDERWATER SUPERCAVITATING HIGH-SPEED BODIES TEST FACILITY

VERTICAL VIEW



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(c)



Supercavitating bullet

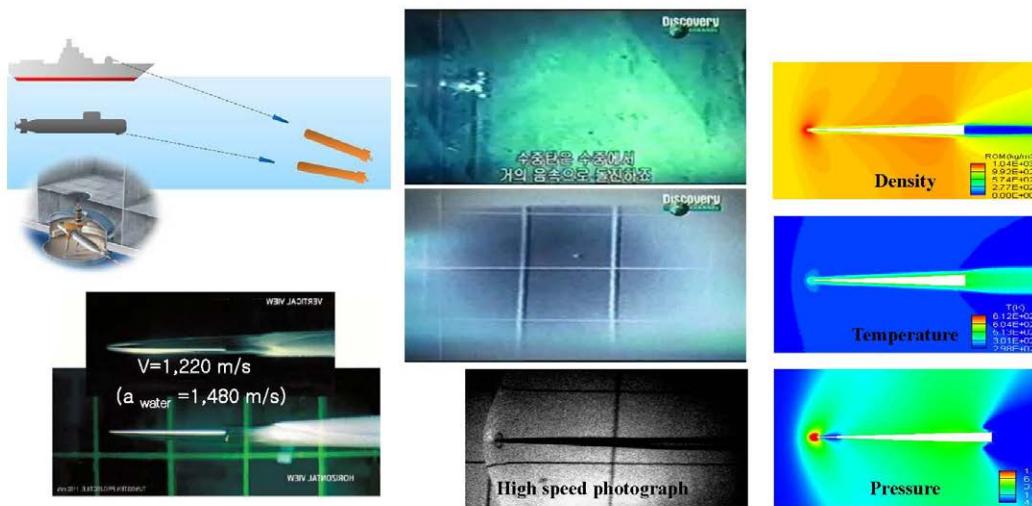


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Supercavitating bullet

 High-Speed Underwater Bullet : $U_\infty = 1,540 \text{ km/h}$ ($M_\infty = 1.03$); $P_\infty = 152.0 \text{ kPa}$ (Depth : 4m); $T_\infty = 27^\circ\text{C}$
- AHSUM (Adaptable High-Speed Underwater Munitions)



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지배 방정식 (Governing Equation)

Continuity Equation

$$\frac{\partial}{\partial t}(Y_L \rho_m) + \frac{\partial}{\partial x}(Y_L \rho_m u) + \frac{\partial}{\partial y}(Y_L \rho_m v) + \frac{\partial}{\partial z}(Y_L \rho_m w) = [\dot{m}_p^+ + \dot{m}_p^-] + [\dot{m}_T^+ + \dot{m}_T^-]$$

$$\frac{\partial}{\partial t}(Y_v \rho_m) + \frac{\partial}{\partial x}(Y_v \rho_m u) + \frac{\partial}{\partial y}(Y_v \rho_m v) + \frac{\partial}{\partial z}(Y_v \rho_m w) = -[\dot{m}_p^+ + \dot{m}_p^-] - [\dot{m}_T^+ + \dot{m}_T^-]$$

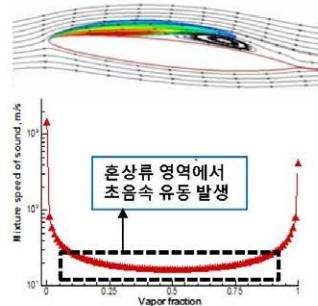
$$\frac{\partial}{\partial t}(Y_g \rho_m) + \frac{\partial}{\partial x}(Y_g \rho_m u) + \frac{\partial}{\partial y}(Y_g \rho_m v) + \frac{\partial}{\partial z}(Y_g \rho_m w) = 0$$

Phase change due to pressure : cavitation

Phase change due to temperature

$$\dot{m}_T^+ = C_{rv} \rho_v \alpha_v \max\left(\frac{T_v - T}{T_v}, 0\right)$$

$$\dot{m}_T^- = C_{rl} \rho_L \alpha_L \min\left(\frac{T_v - T}{T_v}, 0\right)$$



Momentum Equation

$$\frac{\partial}{\partial t}(\rho_m u) + \frac{\partial}{\partial x}(\rho_m u^2) + \frac{\partial}{\partial y}(\rho_m uv) + \frac{\partial}{\partial z}(\rho_m uw) = -\bar{\beta}_p \frac{\partial p}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{xy}}{\partial y} + \rho_m g_x$$

$$\frac{\partial}{\partial t}(\rho_m v) + \frac{\partial}{\partial x}(\rho_m vu) + \frac{\partial}{\partial y}(\rho_m v^2) + \frac{\partial}{\partial z}(\rho_m vw) = -\bar{\beta}_p \frac{\partial p}{\partial y} + \frac{\partial \tau_{yx}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{yz}}{\partial z} + \rho_m g_y$$

$$\frac{\partial}{\partial t}(\rho_m w) + \frac{\partial}{\partial x}(\rho_m uw) + \frac{\partial}{\partial y}(\rho_m vw) + \frac{\partial}{\partial z}(\rho_m w^2) = -\bar{\beta}_p \frac{\partial p}{\partial z} + \frac{\partial \tau_{zx}}{\partial x} + \frac{\partial \tau_{zy}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z} + \rho_m g_z$$

Energy Equation

$$\frac{\partial}{\partial t}(\rho_m h_t - \bar{\beta}_p p) + \frac{\partial}{\partial x}(\rho_m h_t u) + \frac{\partial}{\partial y}(\rho_m h_t v) + \frac{\partial}{\partial z}(\rho_m h_t w) = \frac{\partial(u\tau_{xx} + v\tau_{xy} + w\tau_{xz} - q_x)}{\partial x}$$

$$+ \frac{\partial(u\tau_{yx} + v\tau_{yy} + w\tau_{yz} - q_y)}{\partial y} + \frac{\partial(u\tau_{zx} + v\tau_{zy} + w\tau_{zz} - q_z)}{\partial z} - h(\dot{m}_T^+ + \dot{m}_T^-)$$

Phase change induced energy transfer (latent heat)

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지배 방정식 (Governing Equation)

$$\boxed{\Gamma_e} \frac{\partial \hat{Q}}{\partial t} + \boxed{\Gamma_e} \frac{\partial \hat{Q}}{\partial \tau} + \frac{\partial(\hat{E} - \hat{E}_v)}{\partial \xi} + \frac{\partial(\hat{F} - \hat{F}_v)}{\partial \eta} + \frac{\partial(\hat{G} - \hat{G}_v)}{\partial \zeta} = \hat{S}$$

Isothermal

$$\Gamma_e = \begin{pmatrix} 0 & 0 & 0 & 0 & 0 \\ 0 & \rho_m & 0 & 0 & u\Delta\rho_1 \\ 0 & 0 & \rho_m & 0 & v\Delta\rho_1 \\ 0 & 0 & 0 & \rho_m & w\Delta\rho_1 \\ 0 & 0 & 0 & 0 & 1 \end{pmatrix}$$

Fully Compressible

$Y_i \partial_p \rho_m$	0	0	0	$Y_i \partial_T \rho_m$	$-\rho_m + Y_i \partial_{Yv} \rho_m$
$u \partial_p \rho_m$	ρ_m	0	0	$u \partial_T \rho_m$	$u \partial_{Yv} \rho_m$
$v \partial_p \rho_m$	0	ρ_m	0	$v \partial_T \rho_m$	$v \partial_{Yv} \rho_m$
$w \partial_p \rho_m$	0	0	ρ_m	$w \partial_T \rho_m$	$w \partial_{Yv} \rho_m$
$ht \partial_p \rho_m + \rho_m \partial_p h - 1$	$\rho_m u$	$\rho_m v$	$\rho_m w$	$ht \partial_T \rho_m + \rho_m \partial_T h$	$ht \partial_{Yv} \rho_m + \rho_m \partial_{Yv} h$
$Y_i \partial_p \rho_m$	0	0	0	$Y_i \partial_T \rho_m$	$\rho_m + Y_i \partial_{Yv} \rho_m$

$$\Gamma = \begin{pmatrix} 1/\beta^2 & 0 & 0 & 0 & 0 \\ 0 & \rho_m & 0 & 0 & u\Delta\rho_1 \\ 0 & 0 & \rho_m & 0 & v\Delta\rho_1 \\ 0 & 0 & 0 & \rho_m & w\Delta\rho_1 \\ \alpha_r/\beta^2 & 0 & 0 & 0 & 1 \end{pmatrix}$$

$Y_i \partial_p \rho_m$	0	0	0	$Y_i \partial_T \rho_m$	$-\rho_m + Y_i \partial_{Yv} \rho_m$
$u \partial_p \rho_m$	ρ_m	0	0	$u \partial_T \rho_m$	$u \partial_{Yv} \rho_m$
$v \partial_p \rho_m$	0	ρ_m	0	$v \partial_T \rho_m$	$v \partial_{Yv} \rho_m$
$w \partial_p \rho_m$	0	0	ρ_m	$w \partial_T \rho_m$	$w \partial_{Yv} \rho_m$
$ht \partial_p \rho_m + \rho_m \partial_p h - 1$	$\rho_m u$	$\rho_m v$	$\rho_m w$	$ht \partial_T \rho_m + \rho_m \partial_T h$	$ht \partial_{Yv} \rho_m + \rho_m \partial_{Yv} h$
$Y_i \partial_p \rho_m$	0	0	0	$Y_i \partial_T \rho_m$	$\rho_m + Y_i \partial_{Yv} \rho_m$

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지배 방정식 (Governing Equation)

$$\Delta \hat{Q}^{n+1,k} = \left[I + \Delta t \Gamma^{-1} \left(\frac{\partial A}{\partial \xi} + \frac{\partial B}{\partial \eta} + 1.5 \frac{\Gamma_e}{\Delta t} - S \right) \right] \Delta \hat{R}^{n+1,k}$$

$$\Delta \hat{Q}^{n+1,k} = \hat{Q}^{n+1,k+1} - \hat{Q}^{n+1,k} \hat{R}^{n+1,k} = \Gamma_e \frac{3\hat{Q}^{n+1,k} - 4\hat{Q}^n + \hat{Q}^{n-1}}{2\Delta t} + \left[\left(\frac{\partial E}{\partial \xi} + \frac{\partial F}{\partial \eta} \right) - \left(\frac{\partial E_v}{\partial \xi} + \frac{\partial F_v}{\partial \eta} \right) + \hat{S} \right]^{n+1,k}$$

- Second-order accurate backward difference for the physical time derivative
- First order upwind for the convective flux terms (implicit part)
- First-order backward difference for the pseudo time derivative
- Upwind Non-MUSCL Total Variation Diminishing (TVD) approach for the convective flux terms (Residual part)
- A second-order central for the viscous flux terms (Residual part)

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Cavitation & Boiling Models

Cavitation Models

Option #1 : Merkle et al. 1998

$$\dot{m}^- = \frac{C_{dest} \rho_l \alpha_l \min[0, p - p_v]}{(\rho_l U_\infty^2 / 2) t_\infty}$$

$$\dot{m}^+ = \frac{C_{prod} \rho_v (1 - \alpha_l) \max[0, p - p_v]}{(\rho_l U_\infty^2 / 2) t_\infty}$$

Option #3 : Singhal et al. 2002

$$\dot{m}^- = c_{dest} \frac{\sqrt{k}}{T} \rho_L \rho_v Y_L \frac{dR}{dt}$$

$$\dot{m}^+ = c_{prod} \frac{\sqrt{k}}{T} \rho_L \rho_v Y_v \frac{dR}{dt}$$

Option #4 : Yuan et al. 2003

$$\dot{m}^- = \begin{cases} -\rho_v L (4\pi N)^{1/3} (3\alpha_v)^{2/3} \sqrt{\frac{2|p_v - p|}{3}} & \text{if } p \leq p_v \text{ and } \alpha_v < 1 \\ 0 & \text{if } p > p_v \text{ or } \alpha_v = 1 \end{cases}$$

$$\dot{m}^+ = \begin{cases} \rho_v L (4\pi N)^{1/3} (3\alpha_v)^{2/3} \sqrt{\frac{2|p_v - p|}{3}} & \text{if } p \geq p_v \\ 0 & \text{if } p < p_v \end{cases}$$

Option #2 : Lindau et al. 2002

$$\dot{m}^- = \frac{C_{dest} \rho_v \alpha_l \min[0, p - p_v]}{(\rho_l U_\infty^2 / 2) t_\infty}$$

$$\dot{m}^+ = \frac{C_{prod} \rho_v \alpha_l^2 (1 - \alpha_l)}{t_\infty}$$

Option #5 : Merkle et al. 2006

$$\dot{m}^- = -k_v \frac{\rho_v \alpha_l}{t_\infty} \min \left\{ 1, \max \left(\frac{(p_v - p)}{k_p p_v}, 0 \right) \right\}$$

$$\dot{m}^+ = k_l \frac{\rho_v \alpha_v}{t_\infty} \min \left\{ 1, \max \left(\frac{(p - p_v)}{k_p p_v}, 0 \right) \right\}$$

Boiling Model

Lee's boiling model

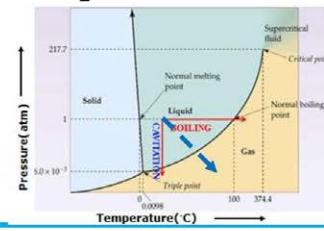
$$\dot{m}_T^+ = C_v \rho_v \alpha_v \max \left(\frac{T_v - T}{T_v}, 0 \right)$$

$$\dot{m}_T^- = C_u \rho_u \alpha_u \min \left(\frac{T_v - T}{T_v}, 0 \right)$$

PNU boiling model(based Merkle model), 2014

$$\dot{m}_T^+ = \frac{C_{Tdest} \rho_L \alpha_L}{\frac{1}{2} \rho_\infty U_\infty t_\infty} \min(T_{sat} - T, 0)$$

$$\dot{m}_T^- = \frac{C_{Tprod} \rho_v \alpha_v}{\frac{1}{2} \rho_\infty U_\infty t_\infty} \max(T_{sat} - T, 0)$$



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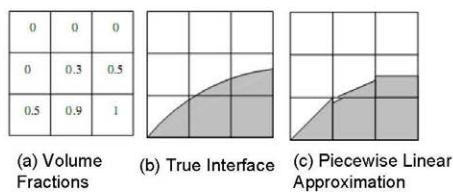


Numerical Methods

VOF MODEL + Multi phase Code

$$\frac{\partial \alpha}{\partial t} + \frac{\partial}{\partial x}(u\alpha) + \frac{\partial}{\partial y}(v\alpha) = 0$$

$$\frac{1}{J} \frac{\partial \alpha}{\partial t} + \frac{\partial}{\partial \xi}\left(\frac{1}{J} U\alpha\right) + \frac{\partial}{\partial \eta}\left(\frac{1}{J} V\alpha\right) = 0$$



* AHEM : Advanced Homogeneous Mixture

AHEM Mixture MODEL + Multi phase Code

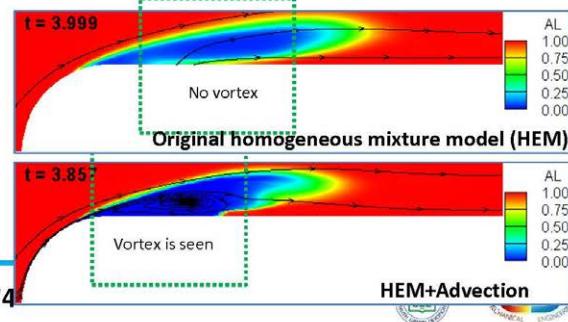
Adding the solution of volume fraction advection equations for both vapor and gaseous mixture to the solution of HEM

+ For vapor phase

$$\frac{\partial \alpha_v}{\partial t} + U \frac{\partial \alpha_v}{\partial \xi} + V \frac{\partial \alpha_v}{\partial \eta} + W \frac{\partial \alpha_v}{\partial \zeta} = - \frac{(\dot{m}^+ + \dot{m}^-)}{\rho_v}$$

+ For non-condensable gaseous mixture

$$\frac{\partial \alpha_g}{\partial t} + U \frac{\partial \alpha_g}{\partial \xi} + V \frac{\partial \alpha_g}{\partial \eta} + W \frac{\partial \alpha_g}{\partial \zeta} = 0$$



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Numerical Methods

VOF equation in Cartesian coordinates

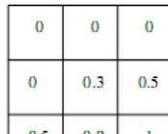
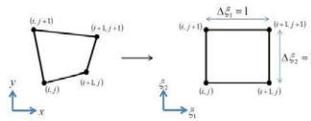
$$\frac{\partial \alpha}{\partial t} + \frac{\partial}{\partial x}(u\alpha) + \frac{\partial}{\partial y}(v\alpha) = 0$$

Transformation to curvilinear coordinates

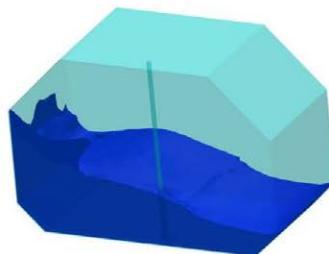
$$\frac{1}{J} \frac{\partial \alpha}{\partial t} + \frac{\partial}{\partial \xi}\left(\frac{1}{J} U\alpha\right) + \frac{\partial}{\partial \eta}\left(\frac{1}{J} V\alpha\right) = 0$$

The contravariant velocities:

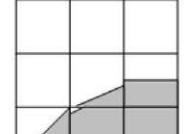
$$U = \xi_x u + \xi_y v; \quad V = \eta_x u + \eta_y v$$



(a) Volume Fractions



(b) True Interface



(c) Piecewise Linear Approximation

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Results and Discussion

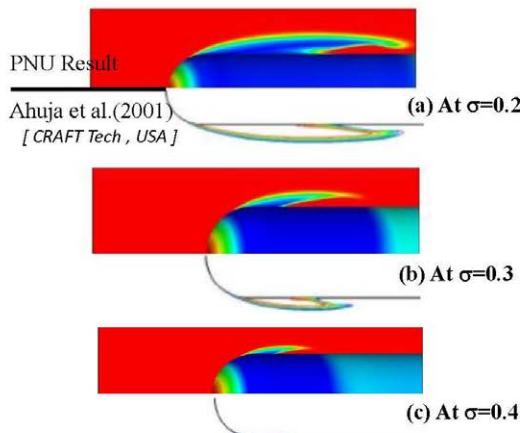
- Natural & Ventilated(Artificial) Cavitation

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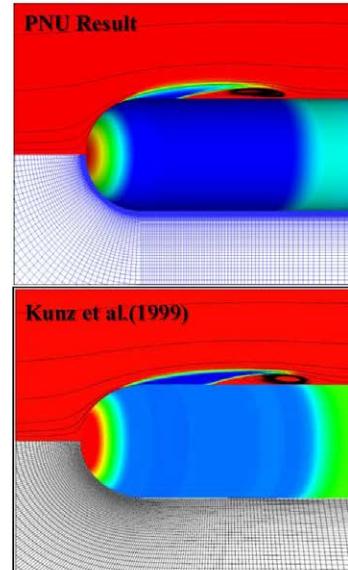


Natural Cavitation

■ Comparison with Ahuja's Result



■ Comparison with Kunz's Result(ONR/ARL)

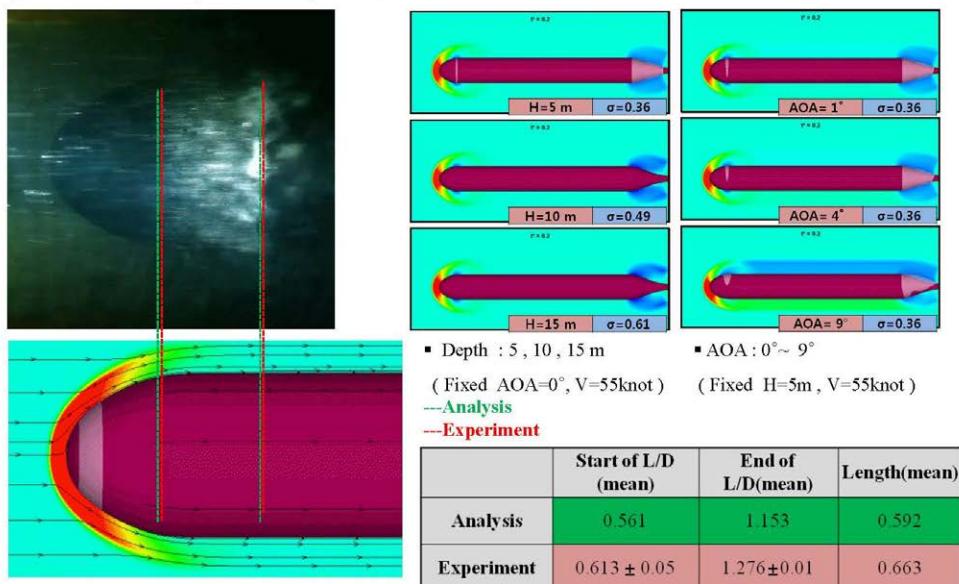


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Natural Cavitation

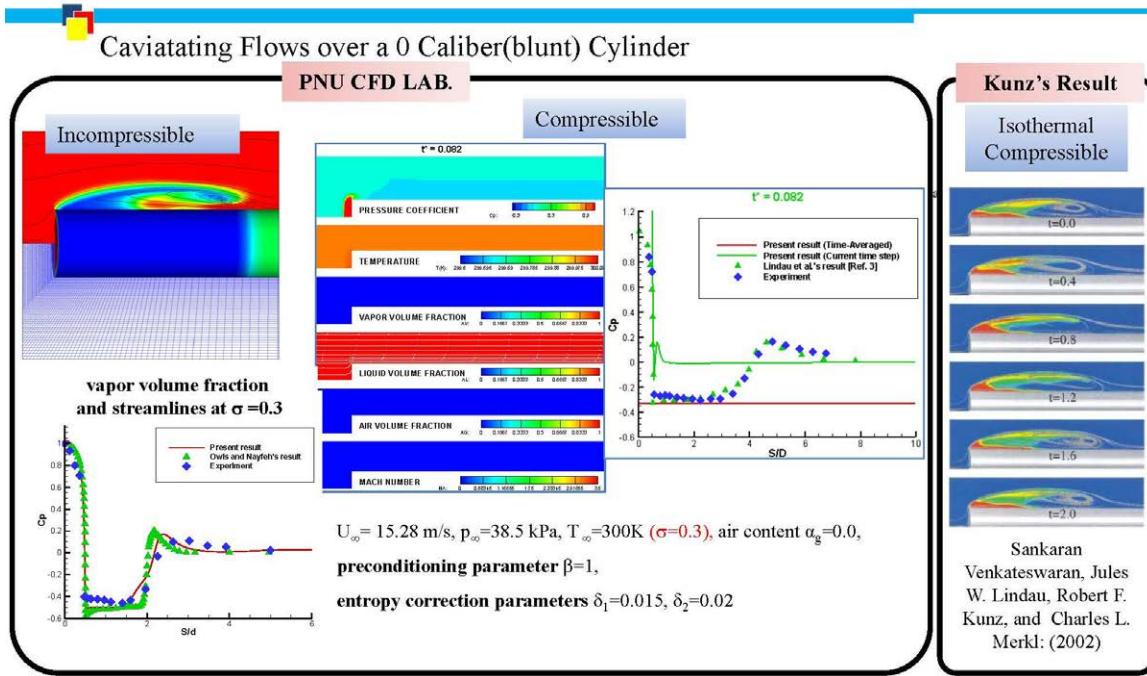
■ Comparison with Experiment (ADD, Korea)



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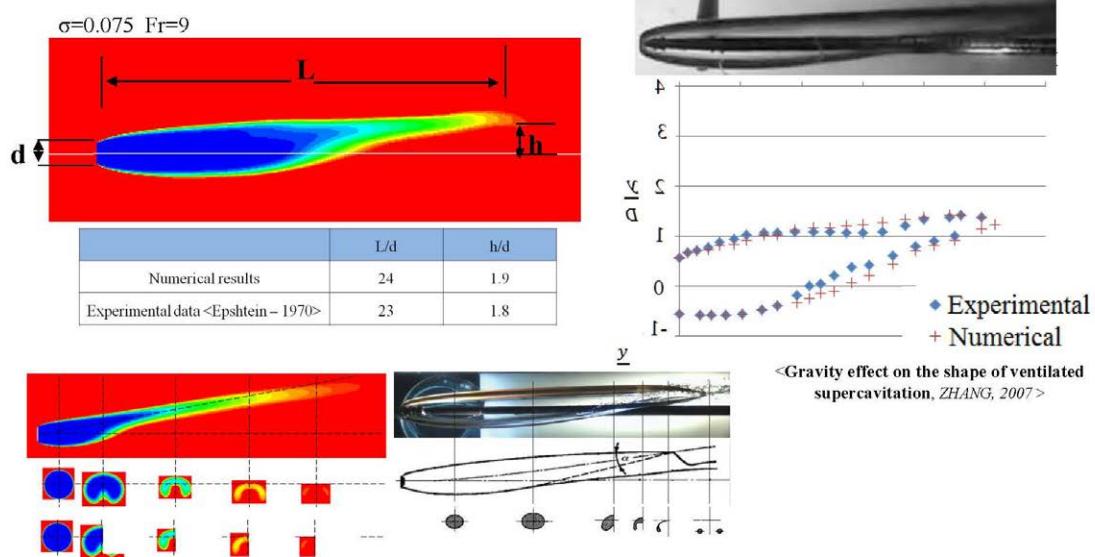
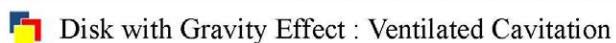
Compressible Effects



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Buoyancy (Gravity) Effect

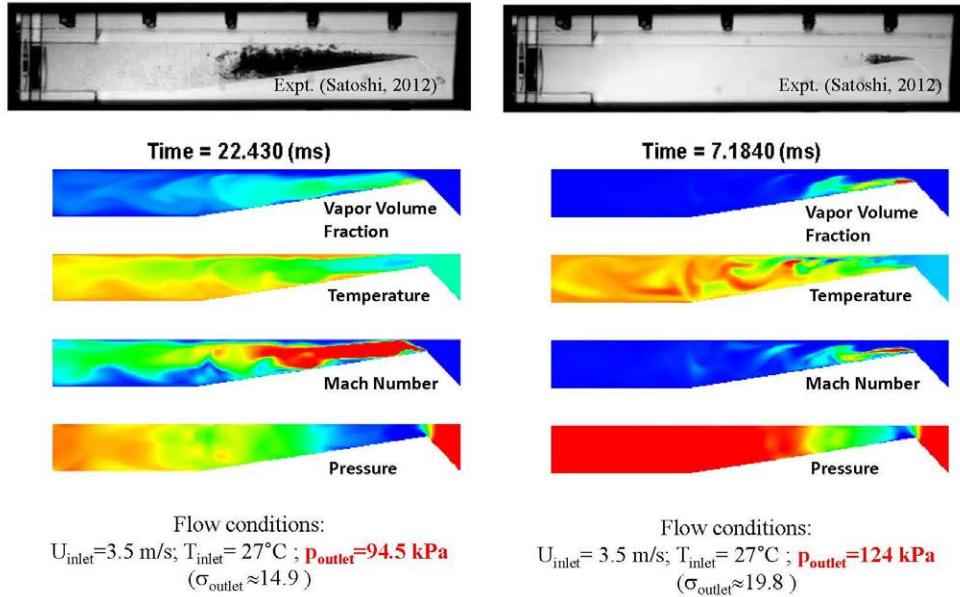


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Nozzle Cavitation

Cavitating Flows in a Nozzle



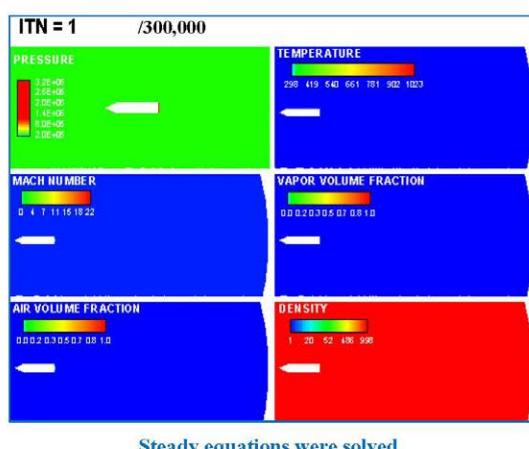
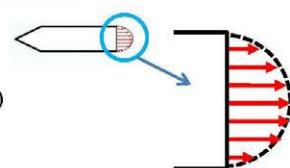
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Compressible Effects

Ventilated Cavitation with Temperarure Difference

- Free stream conditions: $U_\infty = 112 \text{ m/s}$
 $p_\infty = 101.325 \text{ Pa}$; $T_\infty = 25^\circ\text{C}$ (298.15K) ($M_\infty = 0.075$)
- Conditions at the blowhole: $U_{ven} = 392 \text{ m/s}$,
 $p_{ven} = 1.2 \times 10^6 \text{ Pa}$; $T_{ven} = 750^\circ\text{C}$ (1023.15K)



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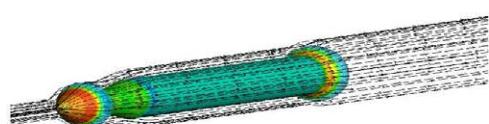
Supercavitating Torpedo

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Barracuda



Without ventilated Cavitation



With ventilated Cavitation



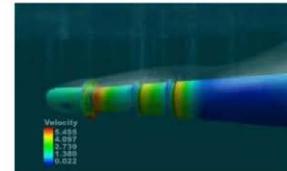
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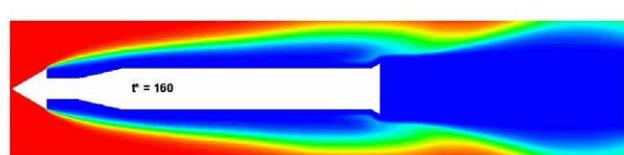
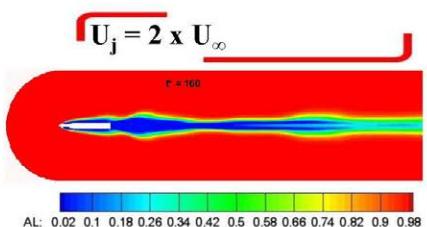
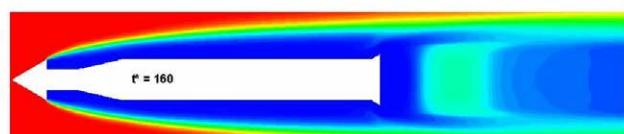
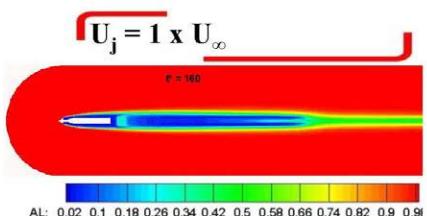
Ventilated Cavitation

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Cavity Instability

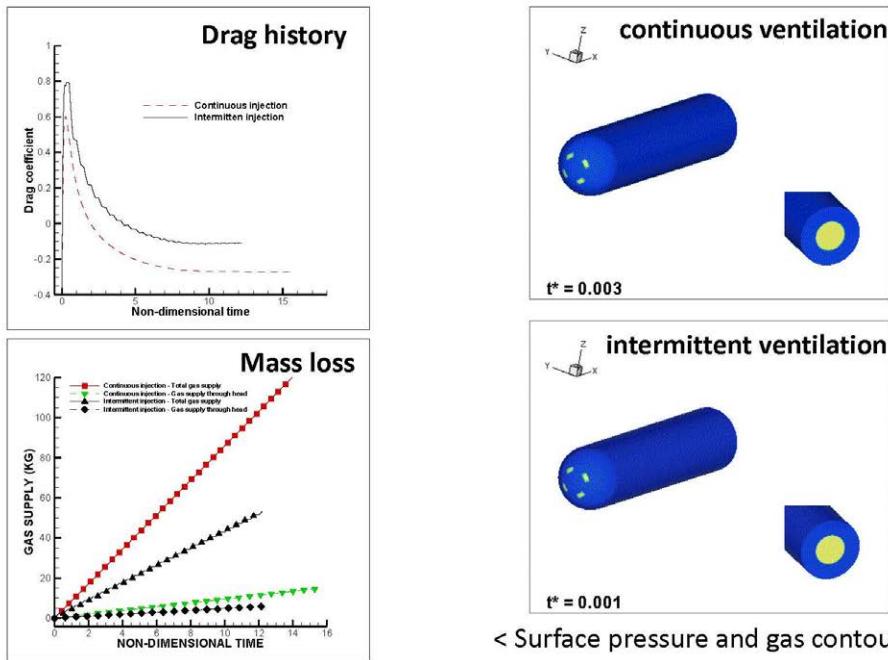


< ONR /ARL >

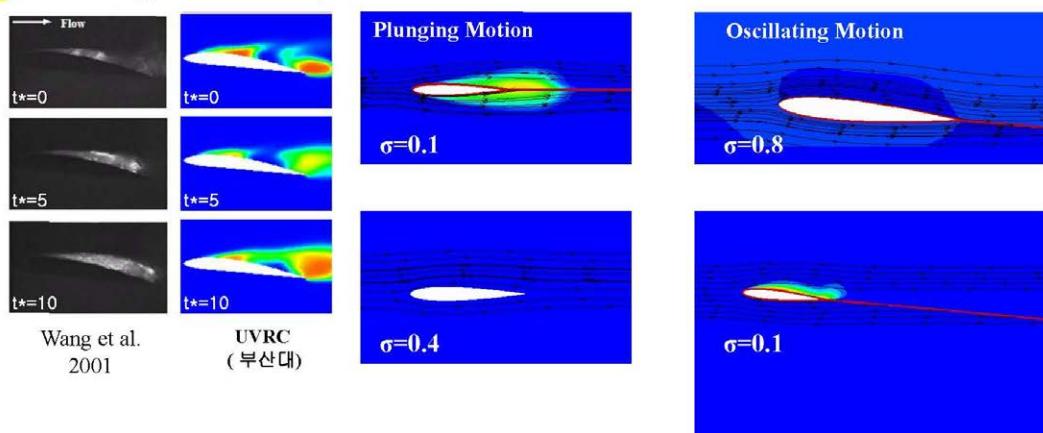


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Ventilated Cavitation - continuous & intermittent ventilation

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**Cavitation over Hydrofoil****Cavitating Flows over Hydrofoil**

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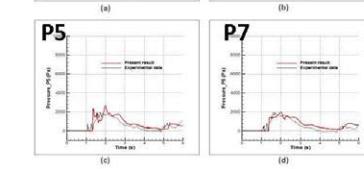
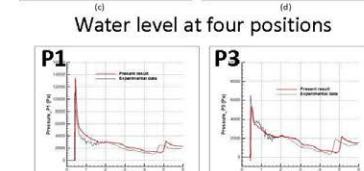
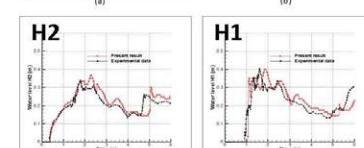
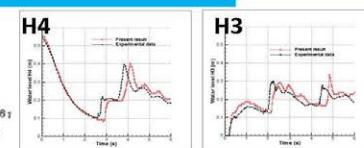
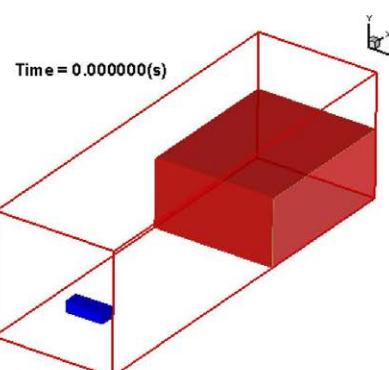
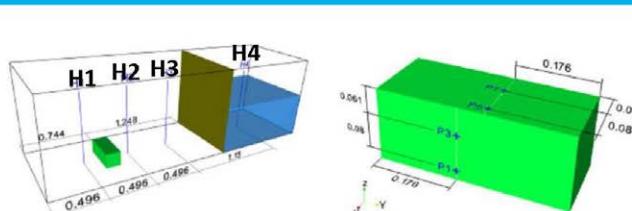
Results and Discussion

- Free Surface Simulations

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Dam-break problem with an object

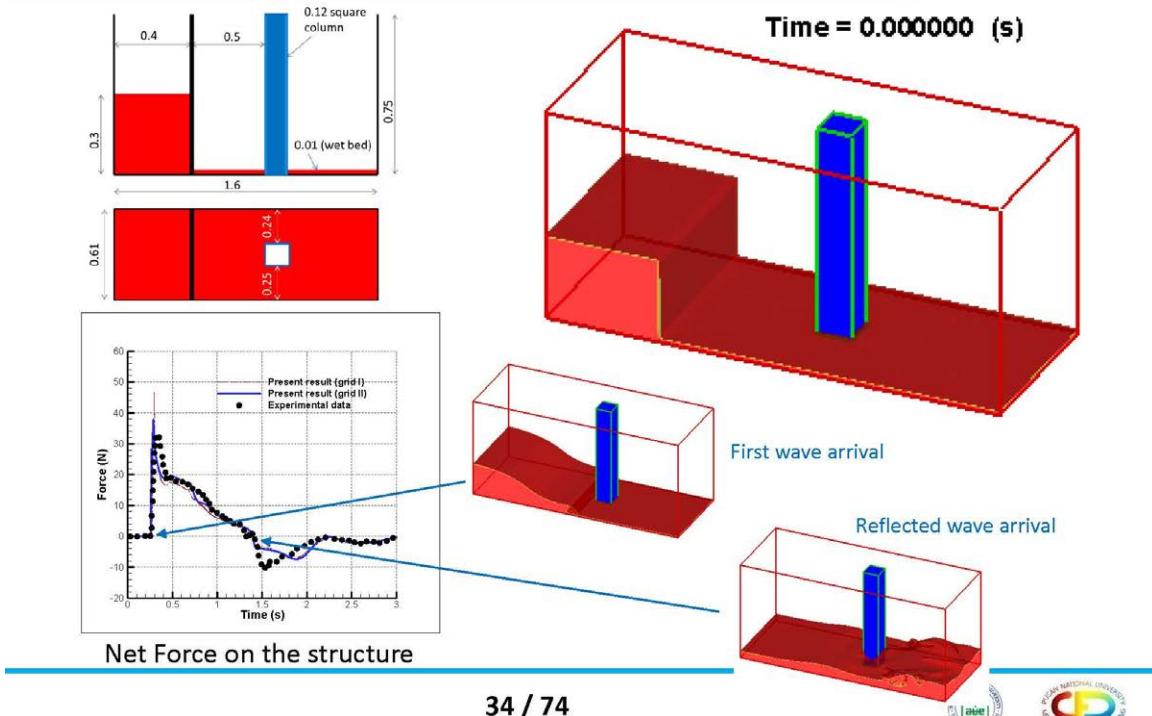


Pressures at four gauges

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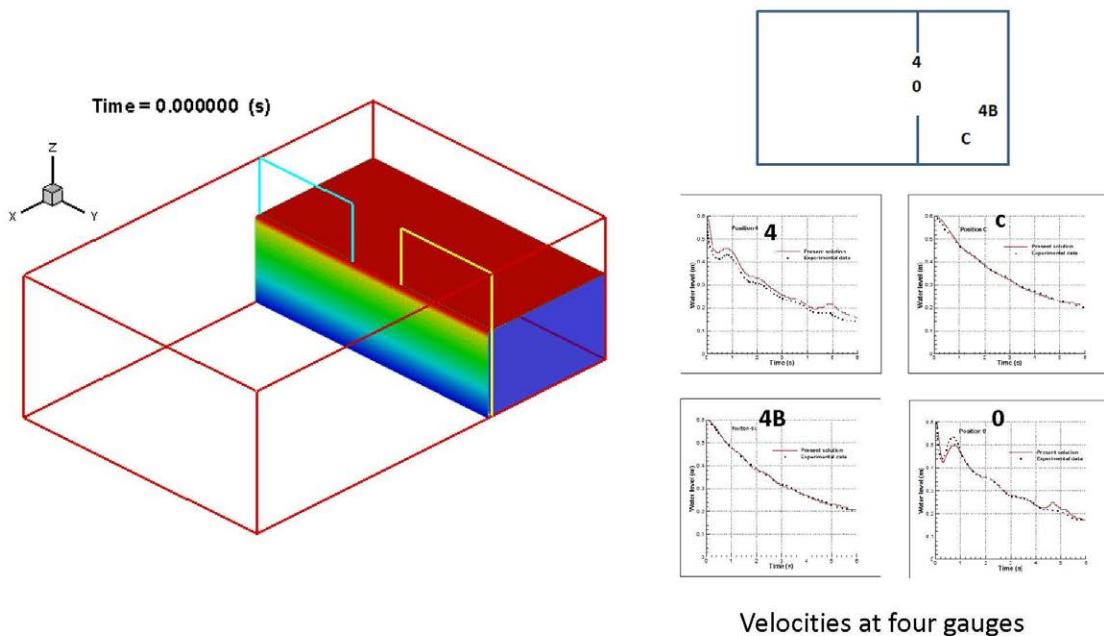
Dam-break problem with an object



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Dam-break problem

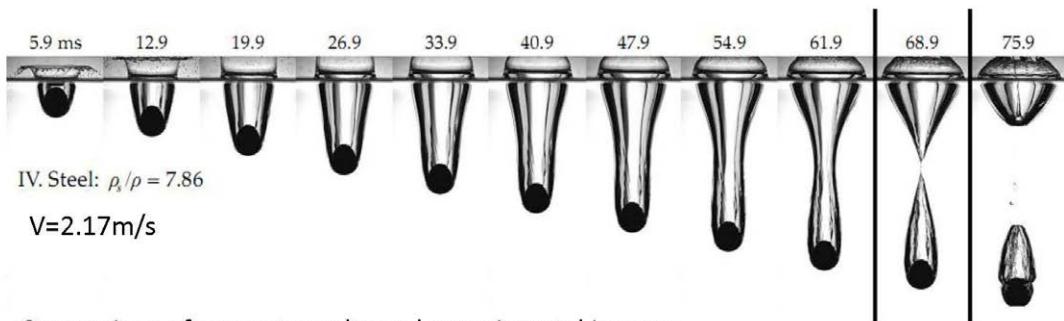


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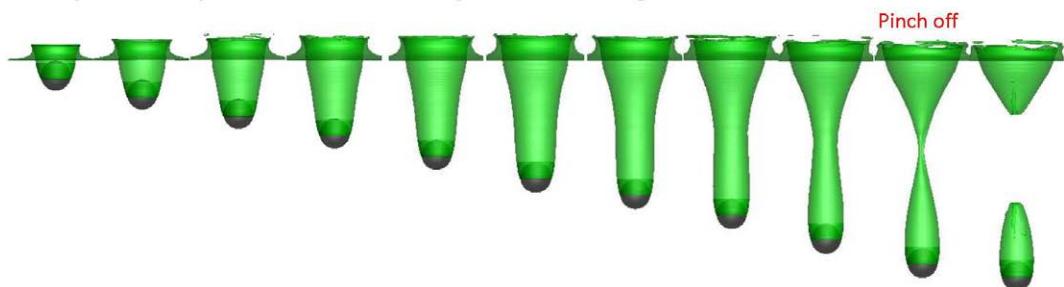


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Simulation of a sphere entering into water using Chimera technique

Comparison of present results and experimental images

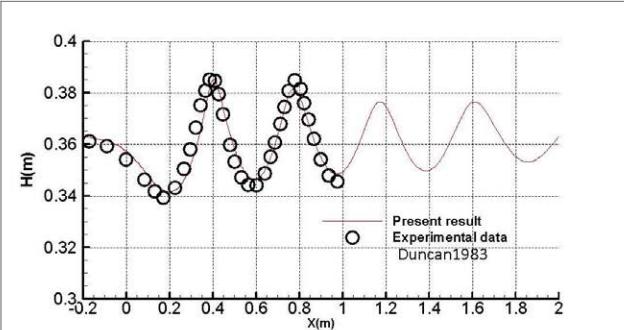
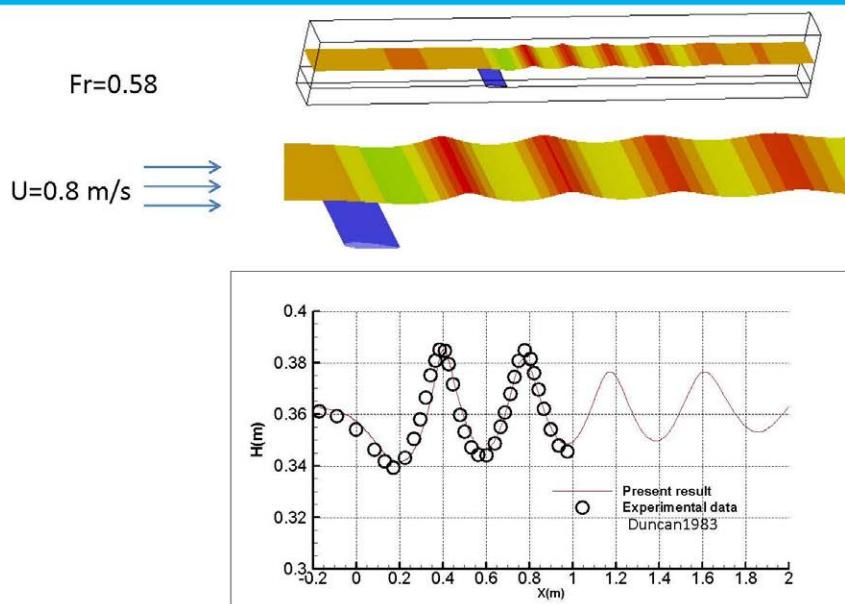


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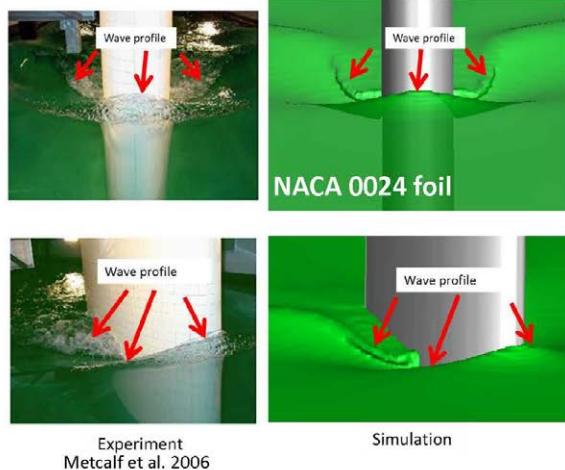
2019.04.23

Steady Free Surface Flows about hydrofoil NACA0012

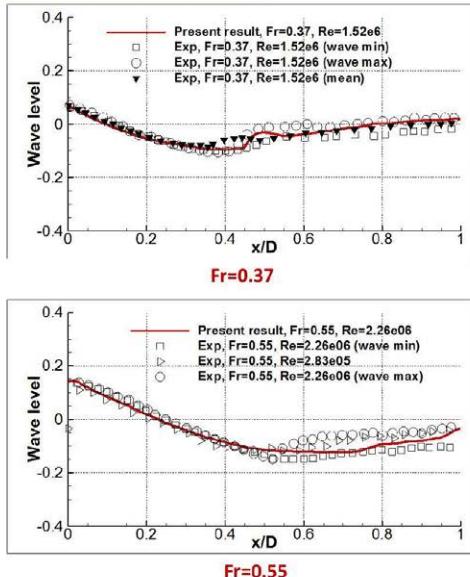
Comparison of wave profile between numerical and experimental results

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Free-surface Wave

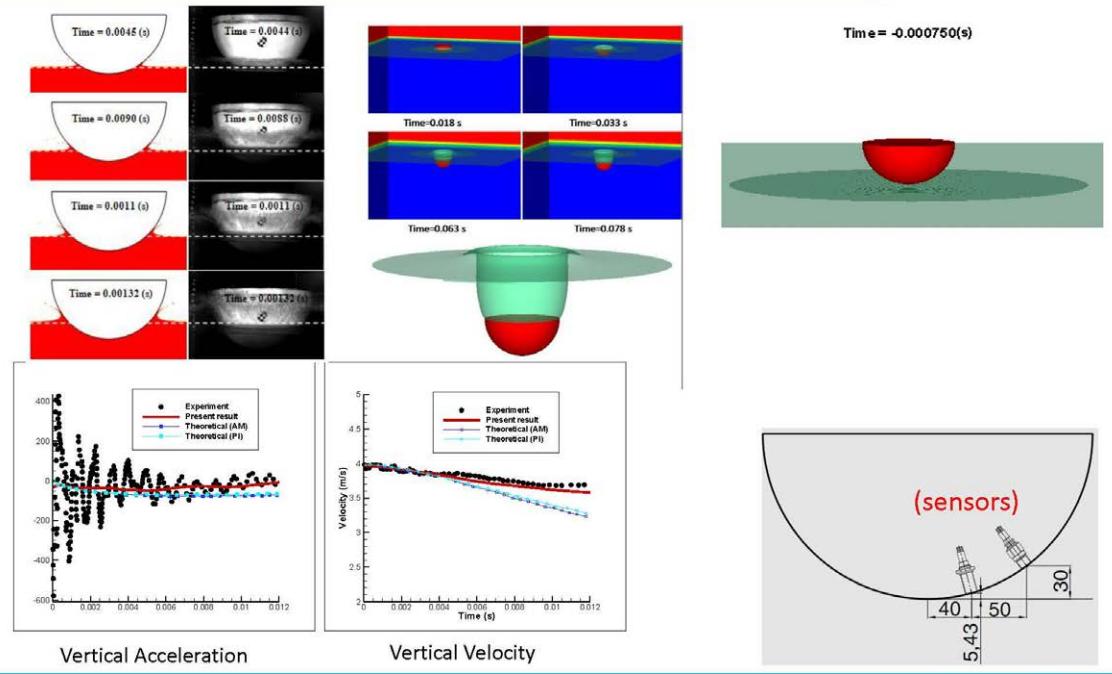
Visual comparison of wave profiles between
CFD and experimental images



Wave profiles and near-field elevations close
to the foil surface

Results and Discussion***- Water Entry Problems***

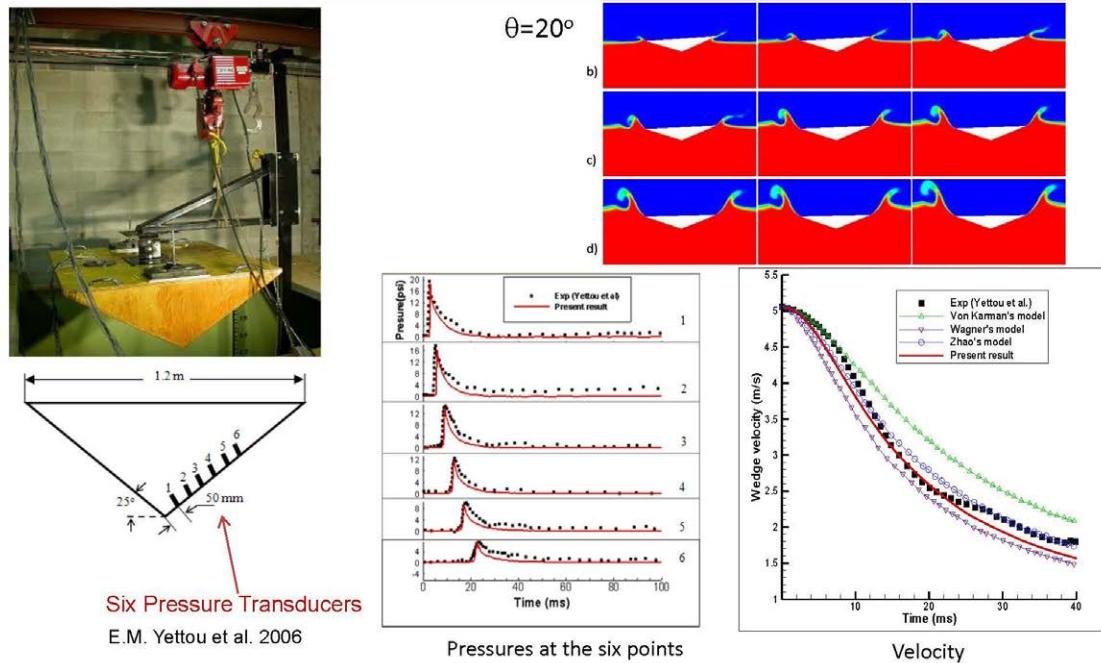
Water Impact Force Analysis



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Water Impact Force Analysis



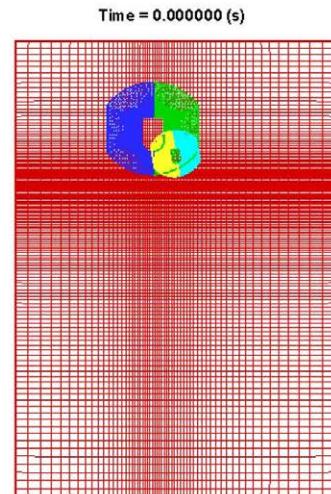
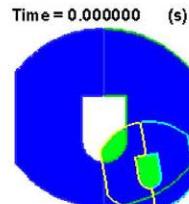
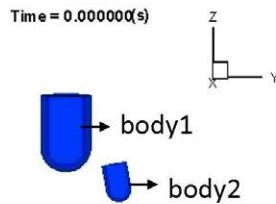
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6 DOF Motion Analysis and Chimera Grid

■ Multi-body entering to the water with multiple Chimera grid

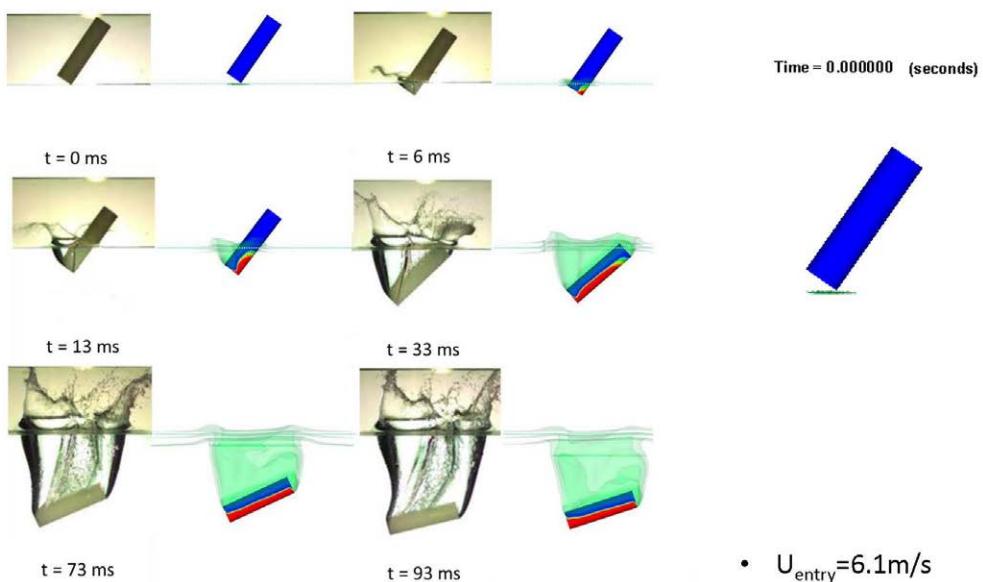
$V_{body1} = 3\text{m/s}$
 $V_{body2} = 5\text{m/s}$
 $\alpha_1 = 0^\circ$
 $\alpha_2 = 10^\circ$



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Simulation of a water entry cylinder with inclined angle

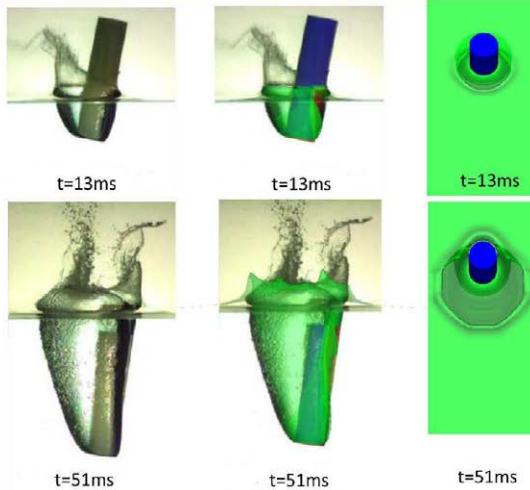
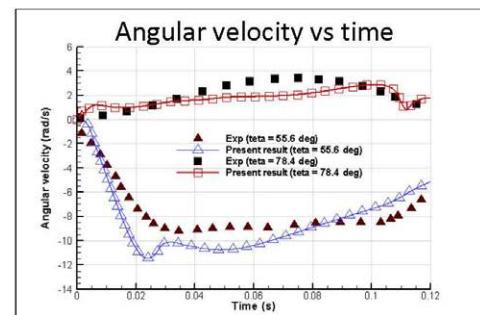
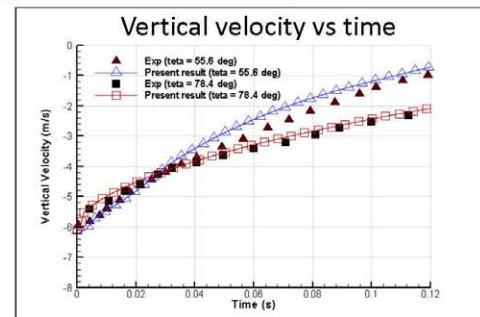


- $U_{entry} = 6.1\text{m/s}$
- Inclined angle = 60°

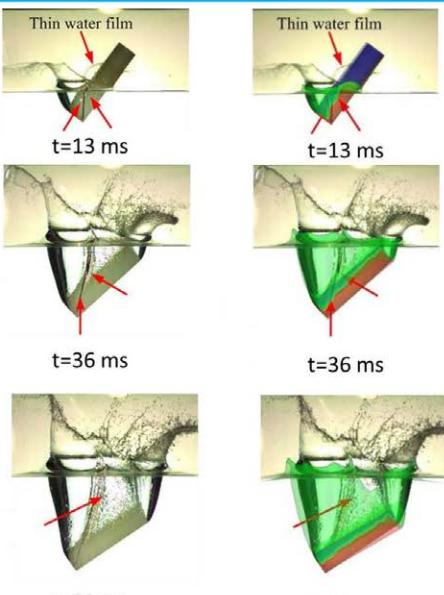
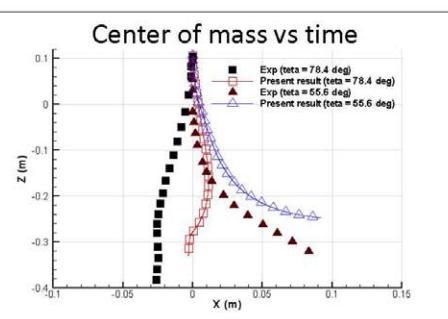
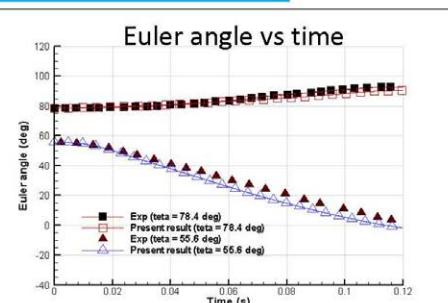
**'Evolution of three-dimensional cavitation following water entry of an inclined cylinder', Zhaoyu Wei, et.al(2012)

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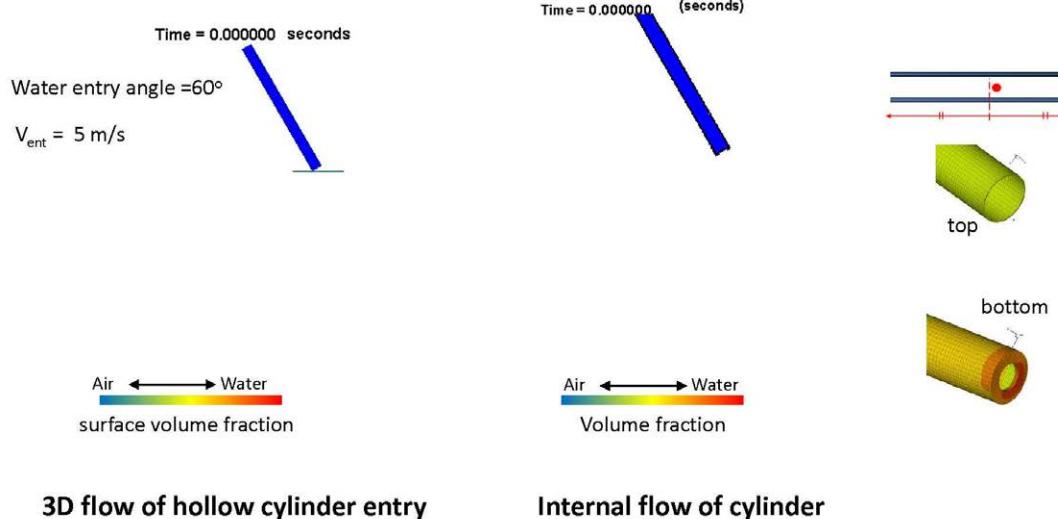
Simulation of a water entry cylinder with inclined angleSagittal snapshots of water entry cylinder at inclined angle of **78.4 degrees**

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Simulation of a water entry cylinder with inclined angleSagittal snapshots of water entry cylinder at inclined angle of **53 degrees**

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6DOF water entry behavior of hollow cylinder

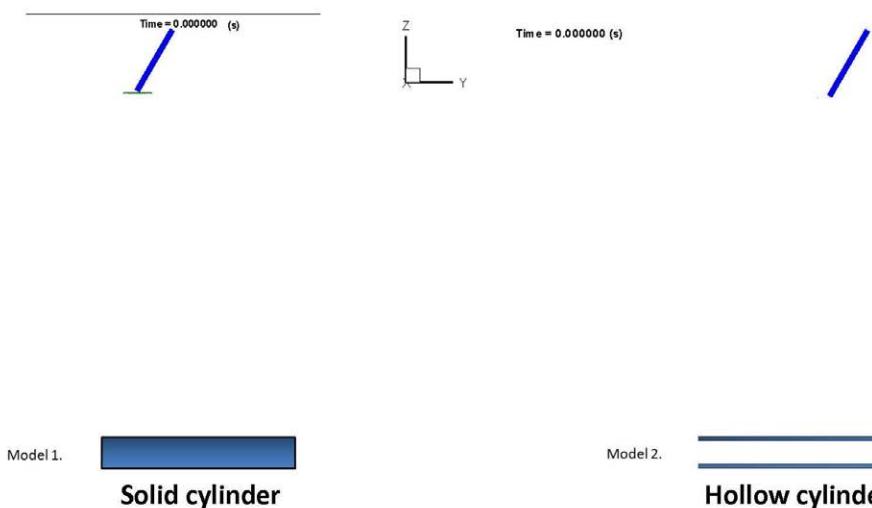


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6DOF water entry behavior of solid/hollow cylinder

- Inclined angles: 60°
- initial entry velocities: 10 m/s



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Ricochet problem

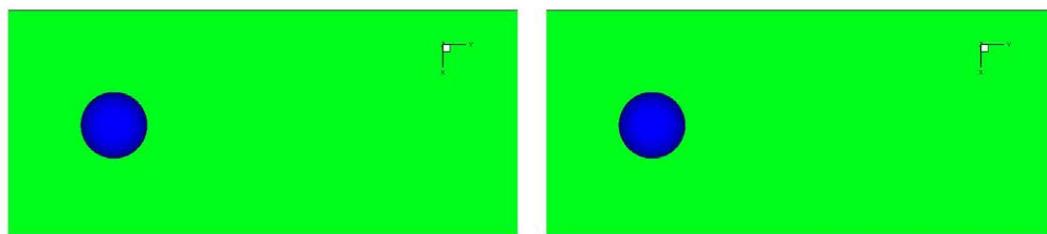
Case1: 10m/s

Time = 0.000000



Case2: 5m/s

Time = 0.000000



Diameter of sphere = 0.025 m
 Density of sphere = water density

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**Results and Discussion**

- *Full Fluids Equation Solver
 for Multiphase Flow Analysis*

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Full Fluids Equations

2D Shock Bubble Interaction

Air/ Helium bubble system

$$\text{Air} \quad \begin{cases} \rho_a = 1.29 \text{ kg/m}^3, u_a = 0 \text{ m/s}, p_a = 10^5 \text{ Pa} \\ \gamma_a = 1.4, \quad \pi_a = 0 \text{ Pa} \end{cases}$$

Helium

$$\begin{cases} \rho_H = 0.167, \quad u_H = 0, \quad p_H = 10^5 \text{ Pa} \\ \gamma_H = 1.67, \quad \pi_H = 0 \text{ Pa} \end{cases}$$

Air/ Nitrogen bubble system

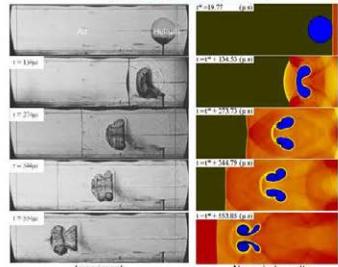
$$\text{Air} \quad \begin{cases} \rho_a = 1.29 \text{ kg/m}^3, u_a = 0 \text{ m/s}, p_a = 10^5 \text{ Pa} \\ \gamma_a = 1.4, \quad \pi_a = 0 \text{ Pa} \end{cases}$$

Nitrogen

$$\begin{cases} \rho_N = 1.25 \text{ kg/m}^3, \quad u_N = 0, \quad p_N = 10^5 \text{ Pa} \\ \gamma_N = 1.4, \quad \pi_N = 0 \text{ Pa} \end{cases}$$

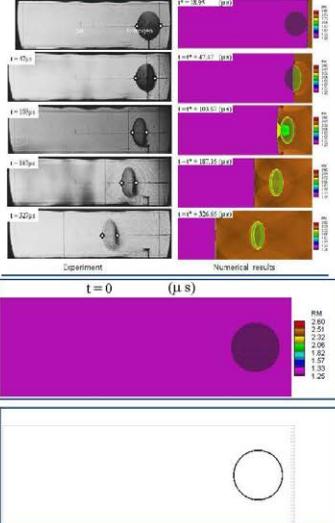
$$\rho_a \approx 10\rho_H$$

AIR-HELIUM SYSTEM



$$\rho \approx \text{same}$$

AIR-NITROGEN SYSTEM



Shock Wave Propagation

Second order HLL scheme with MUSCL interpolation ($\beta=1$)

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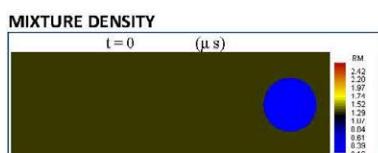


SHOCK BUBBLE INTERACTIONS

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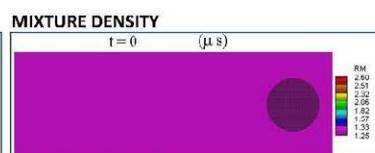
AIR-HELIUM SYSTEM

$$(\rho_{\text{air}}/\rho_{\text{Helium}}=7.72)$$



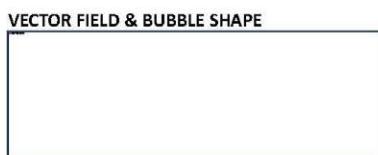
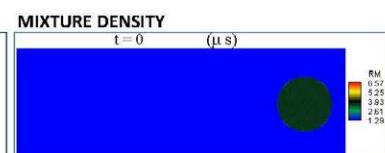
AIR-NITROGEN SYSTEM

$$(\rho_{\text{air}}/\rho_{\text{Nitrogen}}=1.03)$$



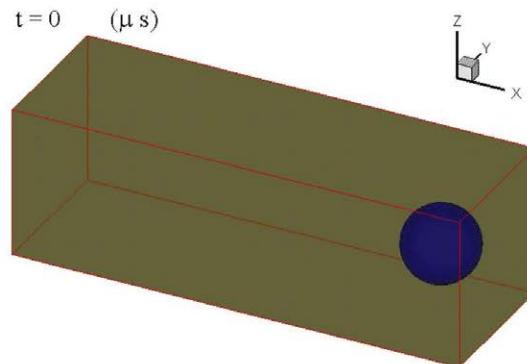
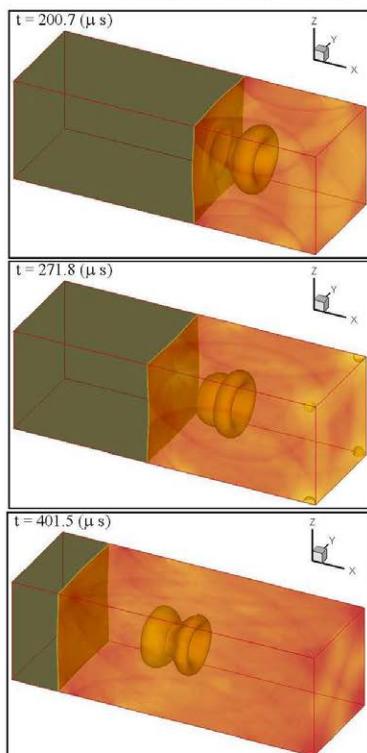
AIR- KRYPTON SYSTEM

$$(\rho_{\text{air}}/\rho_{\text{Krypton}}=0.37)$$



THREE-DIMENSIONAL SHOCK BUBBLE INTERACTION

AIR-HELIUM SYSTEM



Full Fluids Equations

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Richtmeyer-Meshkov Instability

Initial conditions :

$$\begin{cases} \rho_{\text{lightgas}} = 1 \text{ kg/m}^3, \quad p_{\text{lightgas}} = 10^5, \\ u_{\text{lightgas}} = 0 \text{ m/s}, \quad v_{\text{lightgas}} = 0 \text{ m/s} \end{cases}$$

$$\begin{cases} \rho_{\text{heavygas}} = 50 \text{ kg/m}^3, \quad p_{\text{heavygas}} = 10^5 \text{ Pa}, \\ u_{\text{heavygas}} = 0 \text{ m/s}, \quad v_{\text{heavygas}} = 0 \text{ m/s}, \end{cases}$$

$$\begin{cases} \gamma_{\text{lightgas}} = 1.4, \quad \pi_{\text{lightgas}, \infty} = 0 \text{ (Pa)}, \\ \gamma_{\text{heavygas}} = 1.6, \quad \pi_{\text{heavygas}, \infty} = 0 \text{ (Pa)} \end{cases}$$

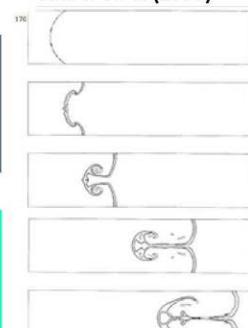


Saurel et. al (2009)

R. Saurel et al./Journal of Computational Physics 228 (2009) 1628–1712



Saurel et. al (1999)



RM 10.00 13.00 15.39 40.00 70.00 100.00 130.00 160.00 180.00 220.00 250.00

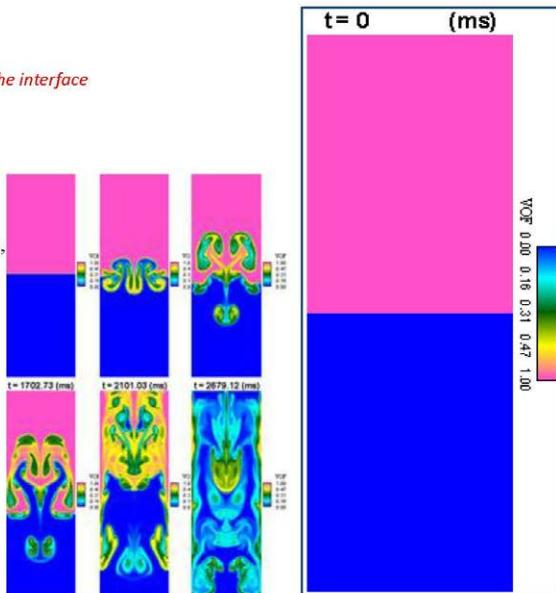
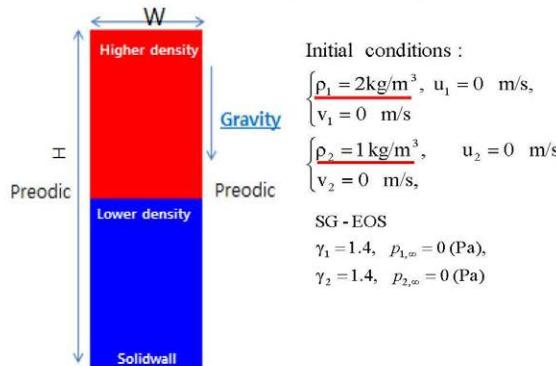
Second order HLL scheme with MUSCL interpolation ($\beta=1$)

Full Fluids Equations

Rayleigh-Taylor Instability

Kelvin-Helmholtz instability may occur :

- If a fluid of high density resting on top of a low-density fluid
- And if a small disturbance, such as a wave, is introduced at the interface



The interface is initially perturbed with

$$v_{\text{dis}} = 0.05 \left[1 + \cos\left(\frac{2\pi x}{W}\right) \right] \left[1 + \cos\left(\frac{2\pi z}{H}\right) \right]$$

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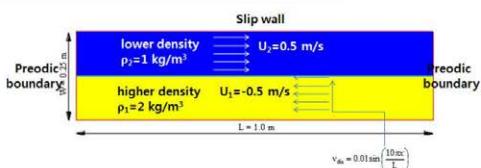


Full Fluids Equations

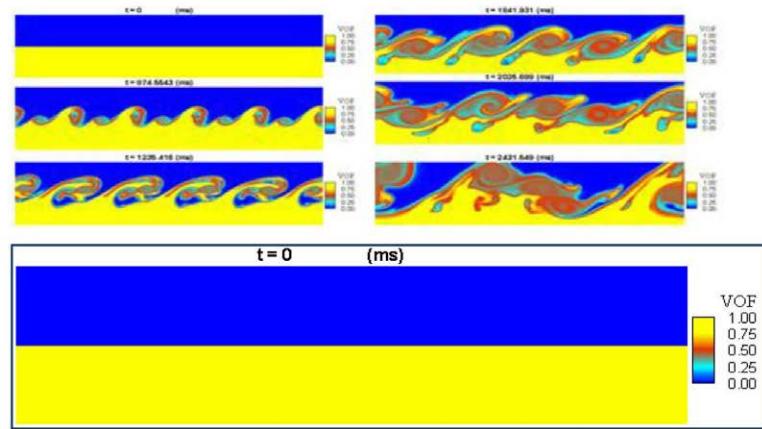
Kelvin-Helmholtz Instability

Initial conditions :

$$\begin{cases} \rho_1 = 2 \text{ kg/m}^3, u_1 = 0 \text{ m/s}, & \text{SG - EOS} \\ v_1 = 0 \text{ m/s} & \gamma_1 = 1.4, p_{1,\infty} = 0 \text{ (Pa)}, \\ \rho_2 = 1 \text{ kg/m}^3, u_2 = 0 \text{ m/s}, & \gamma_2 = 1.4, p_{2,\infty} = 0 \text{ (Pa)} \\ v_2 = 0 \text{ m/s}, & \end{cases}$$



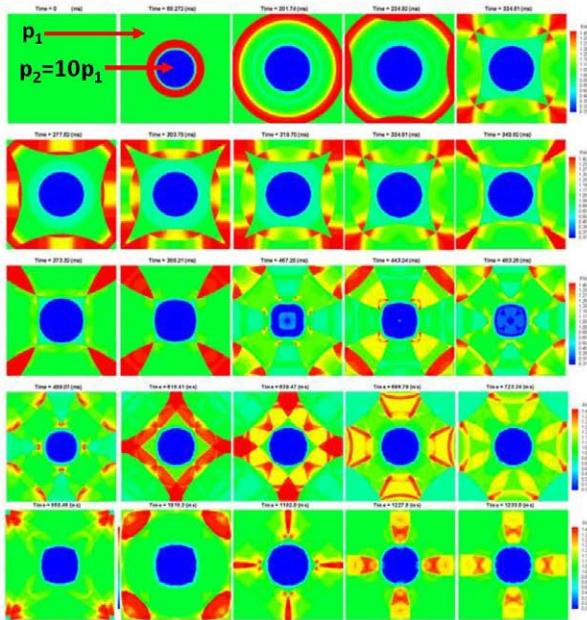
VOID
FRACTION



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Expansion of Spherical Shock



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$$\begin{cases} \rho_1 = 1.0 \text{ kg/m}^3, & p_1 = 1 \text{ Pa}, & u_1 = 0 \text{ m/s}, \\ v_1 = 0 \text{ m/s} \end{cases}$$

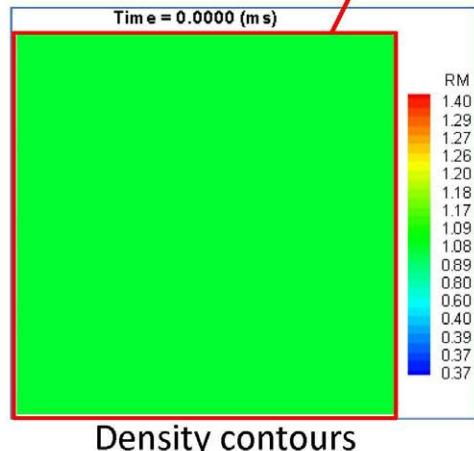
$$\begin{cases} \rho_2 = 1.0 \text{ kg/m}^3, & p_2 = 10 \text{ Pa}, & u_2 = 0 \text{ m/s}, \\ v_2 = 0 \text{ m/s} \end{cases}$$

SG - EOS

$$\gamma_1 = 1.67, \quad p_{1,\infty} = 0 \text{ (Pa)},$$

$$\gamma_2 = 1.67, \quad p_{2,\infty} = 0 \text{ (Pa)}$$

Solid wall



Density contours

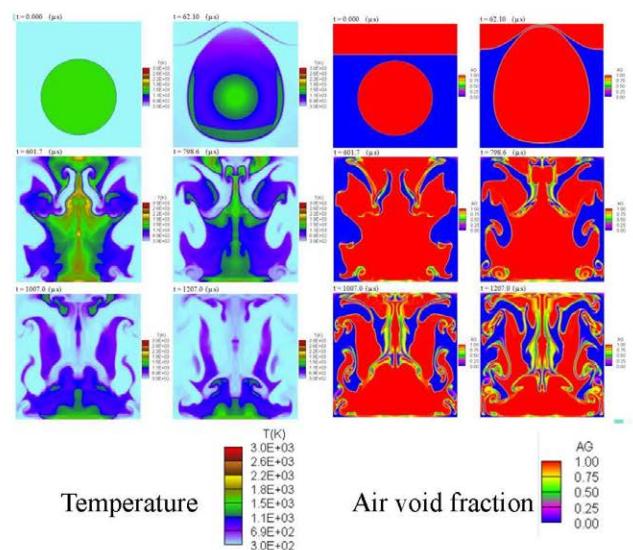
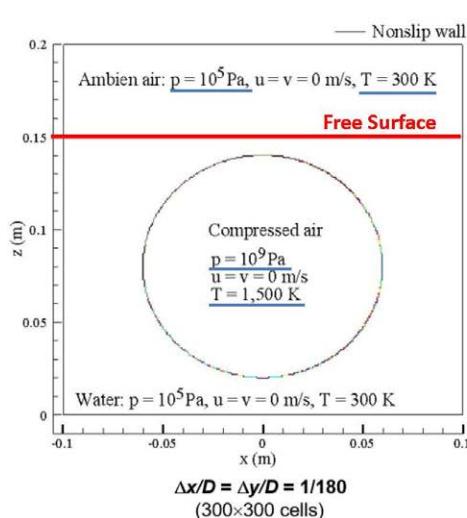
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Underwater Explosion

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To examine the capability for capturing the interface with large jump in pressure, temperature, and density.



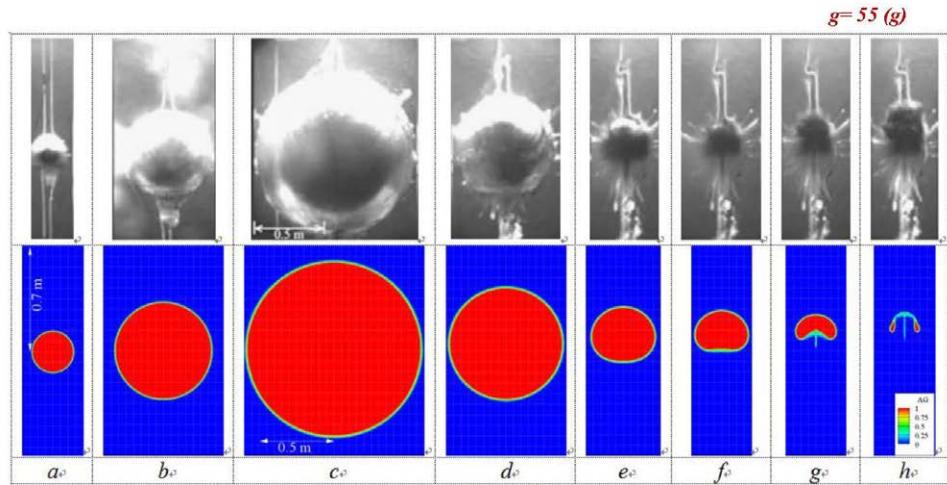
Temperature

Air void fraction

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Underwater Explosion

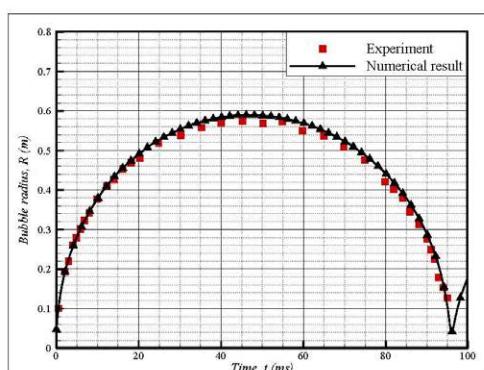


The evolution of bubble shape for case 55g; from the left to right the bubble shape at time, $t = 1, 7, 50, 85, 93, 94, 95$, and 96 ms.

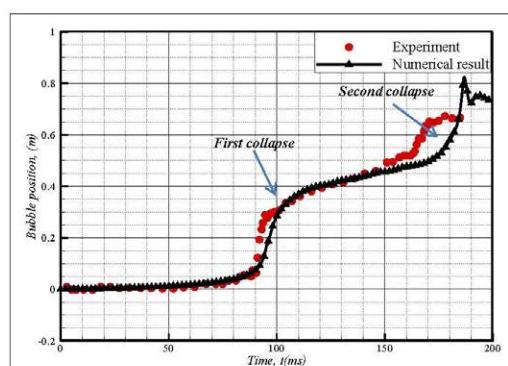
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Underwater Explosion

 $g = 55 \text{ (g)}$ 

The comparison of bubble radius with experiment result for the 55 g case.



The position of the center mass of bubble as function of time

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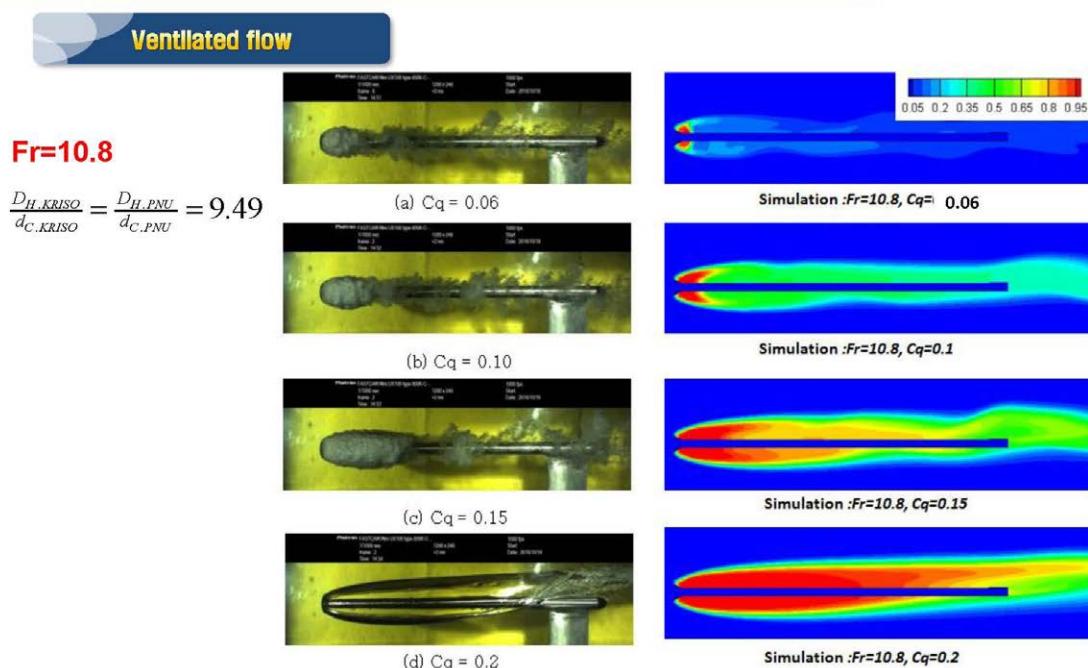
Results and Discussion

- SuperCavitation

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Super Cavitation



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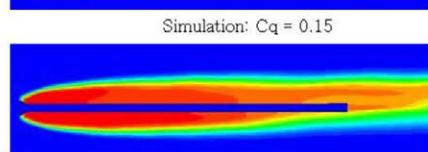
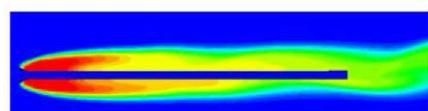
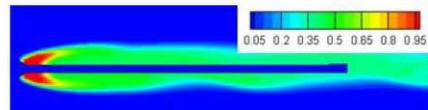
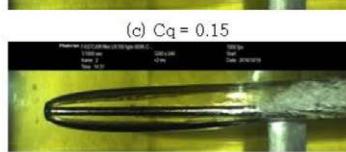
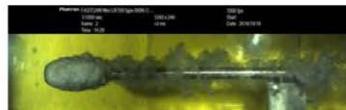


Super Cavitation

Ventilated flow

$Fr=14.4$

$$\frac{D_{H,KRISO}}{d_{C,KRISO}} = \frac{D_{H,PNU}}{d_{C,PNU}} = 9.49$$



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Super Cavitation

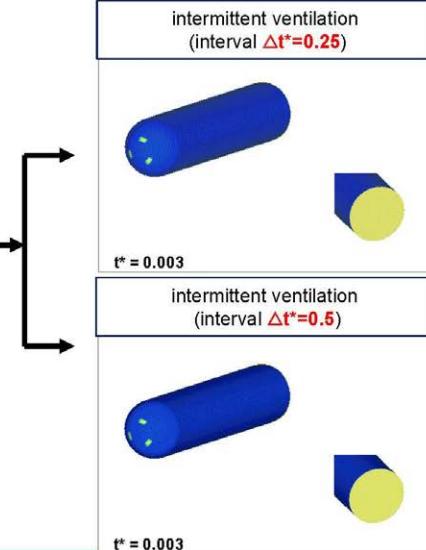
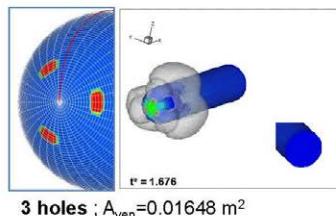
분사 간격 변화

* Flow conditions:

$U_\infty = 50 \text{ m/s}$, $p_\infty = 1.5 \times 10^5 \text{ kPa}$, $T_\infty = 15^\circ\text{C}$

* Ventilation conditions

$T_g = 115^\circ\text{C}$; $Q_g = 36 \text{ kg/s}$; $p_g = 4.0 \times 10^6 \text{ Pa}$



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Super Cavitation

초공동 기술 토의,
2019.04.23

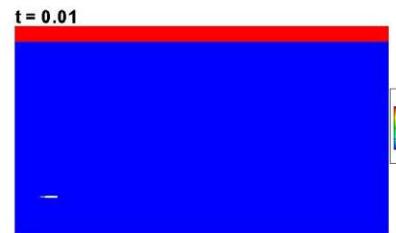
수면 변화

Inlet velocity = 5m/s; Inlet P= 1.00506kPa; Injection velocity = 2m/s;
Injection P = 4.0kPa; Re = 408,482.89; Fr = 17.06;

t = 0.01



10m below the free surface



20m below the free surface

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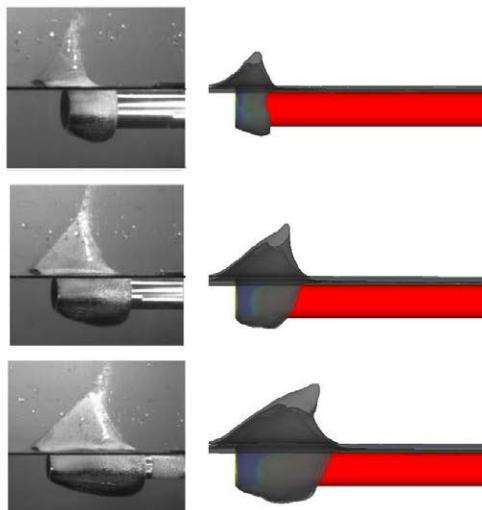


Super Cavitation

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2019.04.23

수면 변화

Velocity: U=19.1 m/s
Diameter: D=37mm
Cav number: 0.54

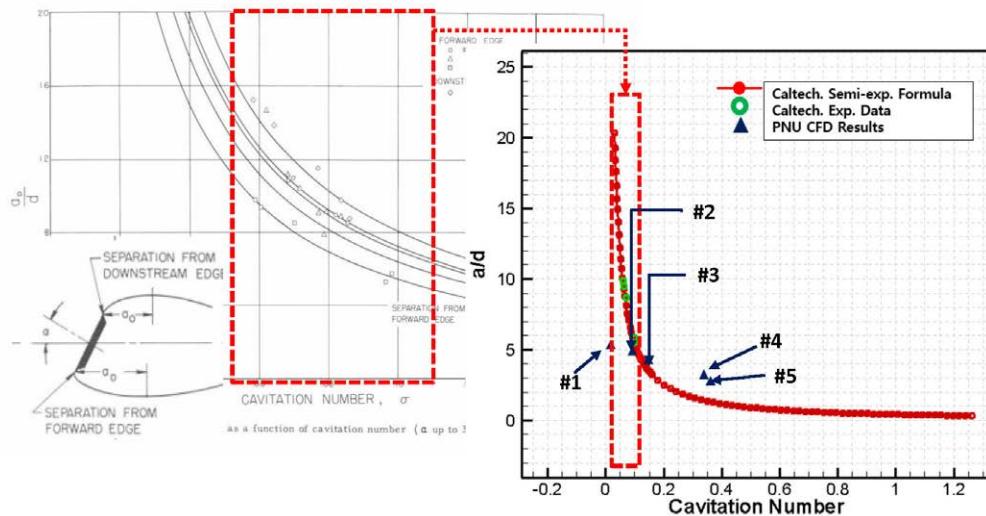


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Super Cavitation

Cavitation Flow In Disk Cavitator with AoA



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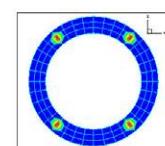
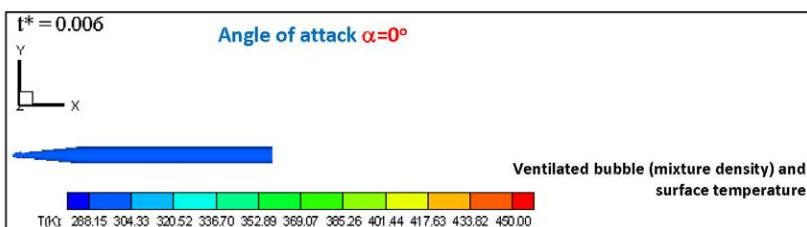


Super Cavitation

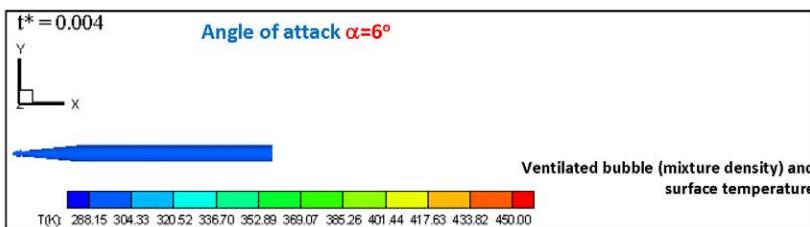
Cavitation Flow In Torpedo with AoA

Flow conditions $U_\infty = 50 \text{ m/s}$, $p_\infty = 101,325 \text{ Pa}$, $T_\infty = 288.15 \text{ K}$

Ventilation conditions $P_{\text{ven}} = 2.5 \text{ MPa}$, $T_{\text{ven}} = 375 \text{ K}$, $U_{\text{ven}} = 390 \text{ m/s}$



Four holes



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Super Cavitation

초공동 기술 토의,
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Cavitation Flow In Cavitator with AoA



Cavitator AoA	Cavity shape (volume fraction)	Point of collapse	Wetted Surface ratio	Drag (cavitaror only)										
-10°		14d_c, 48d_c (Underside)	~5%	<table border="1"> <caption>Drag vs Cavitator AoA</caption> <thead> <tr> <th>Cavitator AoA</th> <th>Drag</th> </tr> </thead> <tbody> <tr><td>-10°</td><td>9.0</td></tr> <tr><td>0°</td><td>9.3</td></tr> <tr><td>10°</td><td>8.9</td></tr> <tr><td>20°</td><td>7.7</td></tr> </tbody> </table>	Cavitator AoA	Drag	-10°	9.0	0°	9.3	10°	8.9	20°	7.7
Cavitator AoA	Drag													
-10°	9.0													
0°	9.3													
10°	8.9													
20°	7.7													
0°		-	0.0											
+10°		14d_c, 52d_c (Upperside)	~5%											
+20°		11d_c (Upperside)	~20%											

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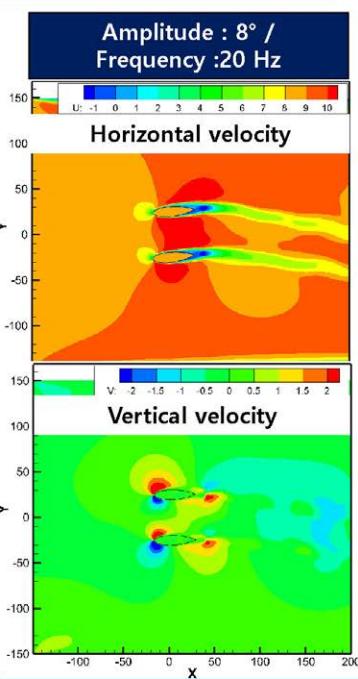
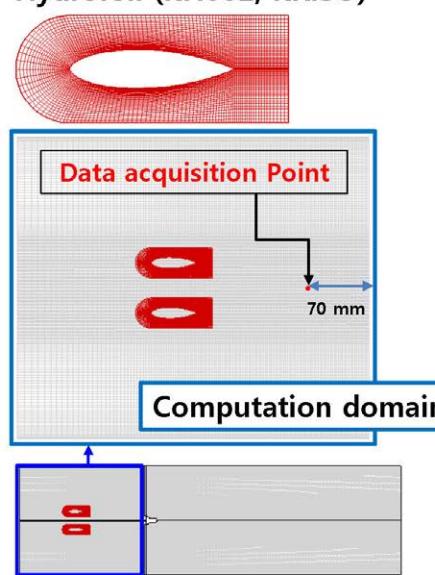


Super Cavitation

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2019.04.23

비정상 외란 해석

Hydrofoil (KH002, KRISO)

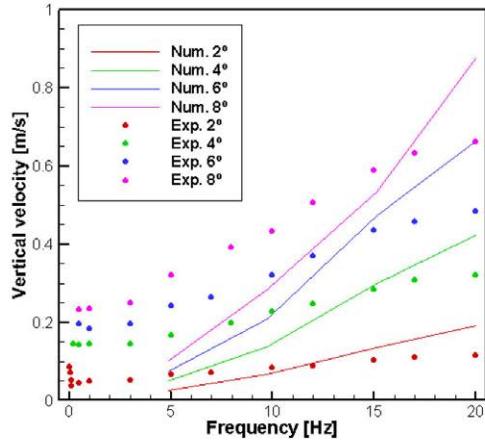


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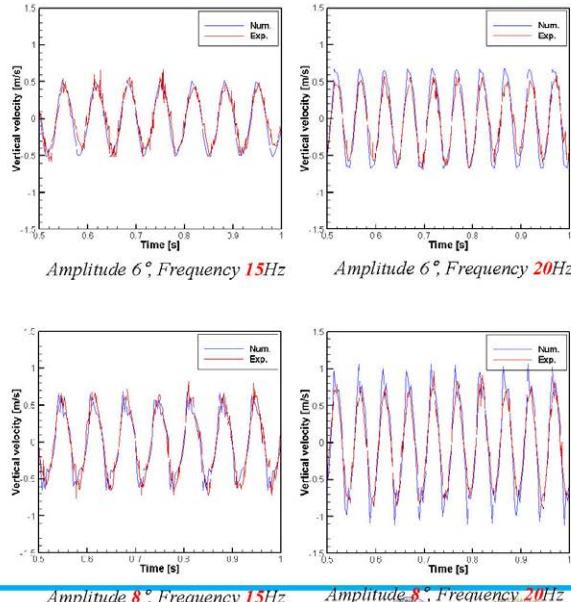


Super Cavitation

비정상 외란 해석



The maximum velocity in vertical direction according to amplitude and frequency

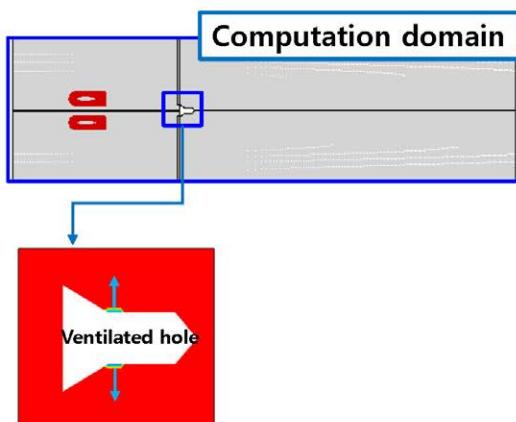


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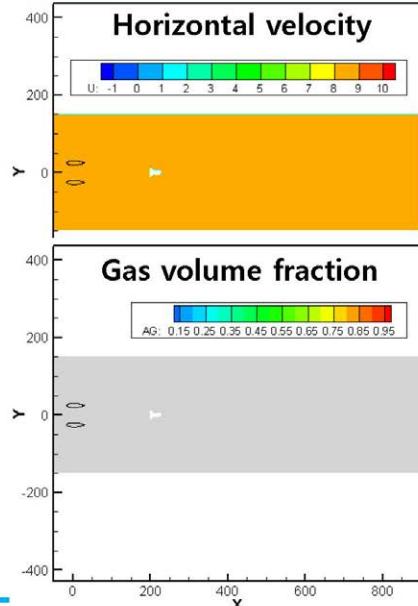
Super Cavitation

비정상 외란 해석



Cavitar with ventilated hole

Amplitude : 8° / Frequency :20 Hz



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Conclusions

초공동 기술 토의,
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- N-S equations based on homogeneous mixture model could be effective method to analyze cavitation
- The in-house code has been successfully developed to capture cavitation phenomena including full compressible effects, non-condensable gas, buoyancy force, temperature difference effects, and ventilated cavitation.
- Free surface was effectively handled by VOF method
- The 6 DOF motion analysis has been done by using chimera grid.
- Also, the in-house code using full fluid equations, not using homogeneous mixture model, has been also successfully developed.

Thank you so much!

Q&A